

**PERFORMANCE OPTIMISATION AND COST REDUCTION THROUGH
ADVANCED PROCESS CONTROL**



Basic Process Control

- Flow pacing
- Feedback control using PID loops
 - pH
 - Free available chlorine

Advanced Process Control (APC)

$$|D(T, \epsilon, a, b)| \leq 2$$

$$\varphi(\sigma_1 t) \varphi(\sigma_2 t) = \varphi(\sqrt{\sigma_1^2 + \sigma_2^2} t)$$

$$P(\alpha) = \frac{\sum_{k=1}^r P_k^* \log_2 \frac{1}{P_k}}{\sum_{k=1}^r P_k^*} \quad c_{ik} \sigma_k^2 = \lambda_i \quad c_{ik} \quad \eta_1 = \sum_{k=1}^r a_{k2} \xi_k \quad \log \varphi(u) = -\frac{\sigma^2 u^2}{2} \quad i^2 = -1; j^2 = -1; k^2 = -1$$

$$A(v) = \sum_{k=1}^r b_k \varphi^*(k v)$$

$$y = \phi(x) = \frac{1}{\sqrt{2\pi}} \int_{-\infty}^{+\infty} e^{-\frac{t^2}{2}} dt \quad S(\alpha, \tau) = \frac{2}{\pi} \int_0^{\pi} \frac{\sin \alpha t}{t} dt \quad P(\eta_{\infty} < x) = F(x)$$

$$W_k = \binom{n}{k} p^k (1-p)^{n-k} \quad P(\eta < y | \xi = x) = \sup_{y', y, y' \in R} P(\eta < y' | \xi = x)$$

$$S_n = A_n U \Pi A_n \quad \lim_{n \rightarrow \infty} \frac{(2n)}{(n+c)} = e^{-2z^2}$$

$$|A_n| = \frac{n!}{2} \left| \int_{|x|>A} f(x) \log_2 \frac{1}{f(x)} dx \right| < \epsilon \quad g^{-1} \cdot g = e \quad f(t|y) = \frac{2e^{-\frac{y^2}{2}}}{\sqrt{2\pi}} \int_{-\infty}^{+\infty} \frac{e^{-\frac{u^2}{2}}}{(1-\frac{y^2}{u^2})^{\frac{3}{2}}} du \quad \Delta N = \sum_{u=1}^N \frac{\epsilon u}{u}$$

$$\int_{+\infty}^{-\infty} dG_k(x) \geq \frac{1}{2} \sum_{k \rightarrow \infty} e^{-\frac{k^2 \pi^2}{2}} = H(k) \quad \prod_{k \leq b} M_i; \bigcup_{i=1}^{n-1} X_n \quad H_r(x) = \frac{G_r(x)}{1+G_r(x)} \quad U_n^{(c)} = \binom{2n}{n} - \binom{2n}{n-c}$$

$$f_{n-1}(t) = \int_0^1 f_n(u) f_1(t-u) du = \frac{2^{n+1} e^{-2t}}{n!} \quad \lim_{t \rightarrow 0} (e^{2t}) = 0 \quad \lim_{n \rightarrow \infty} \frac{f_n(t)}{n} = P_k \quad R = \int_{-\infty}^{+\infty} \varphi(t) dt$$

$$\log \varphi(t) = i \gamma t - c |t|^\alpha [1 + i \beta \frac{t}{|t|} \omega(t, m)] \quad \beta(u) = \sum_{k=1}^r \varphi^*(b_k u) \quad c_{iv} = \sum_{j=1}^r a_{ij} b_{jv} \quad \lim_{n \rightarrow \infty} P \left(\frac{\sum_{k=1}^r (j_{n+1-k} - \log \frac{1}{q})}{\sqrt{1-q}} \right) C_n(\alpha) \geq \frac{n!}{\prod_{k=1}^n n_k(\omega)!} \quad \frac{u}{m} \varphi(t) = \varphi(c \frac{u}{m} t)$$

$$\int_{-\infty}^{+\infty} e^{-\frac{u^2}{2}} du = F(x) \left(\frac{1}{\sqrt{2\pi}} \right)^{-1} \quad |\Psi_5(t)| = \left| \int_{-\infty}^{+\infty} e^{itx} dF(x) \right| \leq \int_{-\infty}^{+\infty} e^{-vx} dF(x) = \varphi_5(iv) \quad g^{-1} N g = \{g^{-1} n g | n \in N\} \quad Q = F^{-1}(c_q) \quad \varphi_n(\alpha) = \frac{P_k^*}{\sum_{j=1}^r P_j^*} \quad P(\Pi_2)$$

$$\prod_{m=1}^r \prod_{l=1}^r \prod_{m-r}$$

$$|X \cup Y| = |X| + |Y| - |X \cap Y| \quad \lim_{n \rightarrow \infty} \frac{1}{n} k_n \left(\frac{x}{\sqrt{n}} \right) = \frac{1}{\sqrt{2\pi}} e^{-\frac{x^2}{2}} \quad P_n(k) = P_{j_0}^{(c)} \quad P \left(\limsup_{n \rightarrow \infty} \frac{|h_n|}{\sqrt{2n \log \log n}} \leq 1 \right) = 1 \quad (q+1) = 1 - \sqrt{1-e^{2it}}$$

$$f: X \rightarrow X \cap W$$

$$Q(A) = \int_A f(x) dP \quad l'(x) = -\log_2 \left(\frac{\sum_{k=1}^r P_k^* \log_2 \frac{1}{P_k}}{\sum_{k=1}^r P_k^*} - \left(\frac{\sum_{k=1}^r P_k^* \log_2 \frac{1}{P_k}}{\sum_{k=1}^r P_k^*} \right)^2 \right) \quad f g(u_i) = f \left(\sum_{j=1}^r a_{ji} v_j \right) = \sum_{j=1}^r a_{ji} \left(\sum_{k=1}^r b_{kj} w_k \right) \left(\frac{2b_j}{2^{2k}} \right) \approx \frac{1}{\sqrt{\pi} b_k}$$

$$q \left(e^{-x} \sqrt{\frac{1-q}{nq}} - 1 \right) = x \sqrt{\frac{q(1-q)}{n}} + o \left(\frac{1}{n} \right) \quad \prod_{k=1}^r \left[g_k \left(\frac{t}{\sqrt{N_0}} \right) \right]^{N_0 \alpha_k} = e^{-\frac{t^2}{2}} \quad P_{jk}^{(m)} = \sum_{l=0}^{\infty} P_{jl}^{(r)} P_{lk}^{(m-r)} \quad \frac{1}{2\pi} \int_{-\infty}^{+\infty} \text{Re} \left\{ \varphi(t) \frac{e^{-ita} - e^{-itb}}{it} \right\} dt$$

$$\liminf_{N \rightarrow \infty} \int_{-\infty}^{+\infty} f_N(x)^\alpha dx \geq \int_{-\infty}^{+\infty} f(x)^\alpha dx \quad \lim_{N \rightarrow \infty} \int_{-A}^{+A} f_N(x) \log_2 \frac{1}{f_N(x)} dx = \int_{-A}^{+A} f(x) \log_2 \frac{1}{f(x)} dx \quad P(|\omega_n| \geq \epsilon) \leq \frac{C_q}{\log N}$$

$$M(\log_2 -1^N) = \int_0^{\infty} (x-1)^N e^{-x} dx \quad N \epsilon_n - \epsilon_n = \binom{2n}{n+bc} = \binom{2n}{n}$$

$$D^2(J_n) \leq \frac{k}{n} + 2k \left(\frac{1}{2} \sum_{k=1}^n R(k) \right) \quad \det(M') = \det(M) + \det(M^*) = \det(M) \quad h(x, y) = \frac{1}{\sqrt{2\pi}} \left[\sqrt{2} e^{-\frac{x^2}{2}} - e^{-xy} \right] \quad |M(\epsilon_n, \epsilon_m)| \leq C_2 \sqrt{\frac{n}{m-n}}$$

APC Examples

- Feed forward control
- Indirect sensors
- Sequential logic control
- Model predictive control





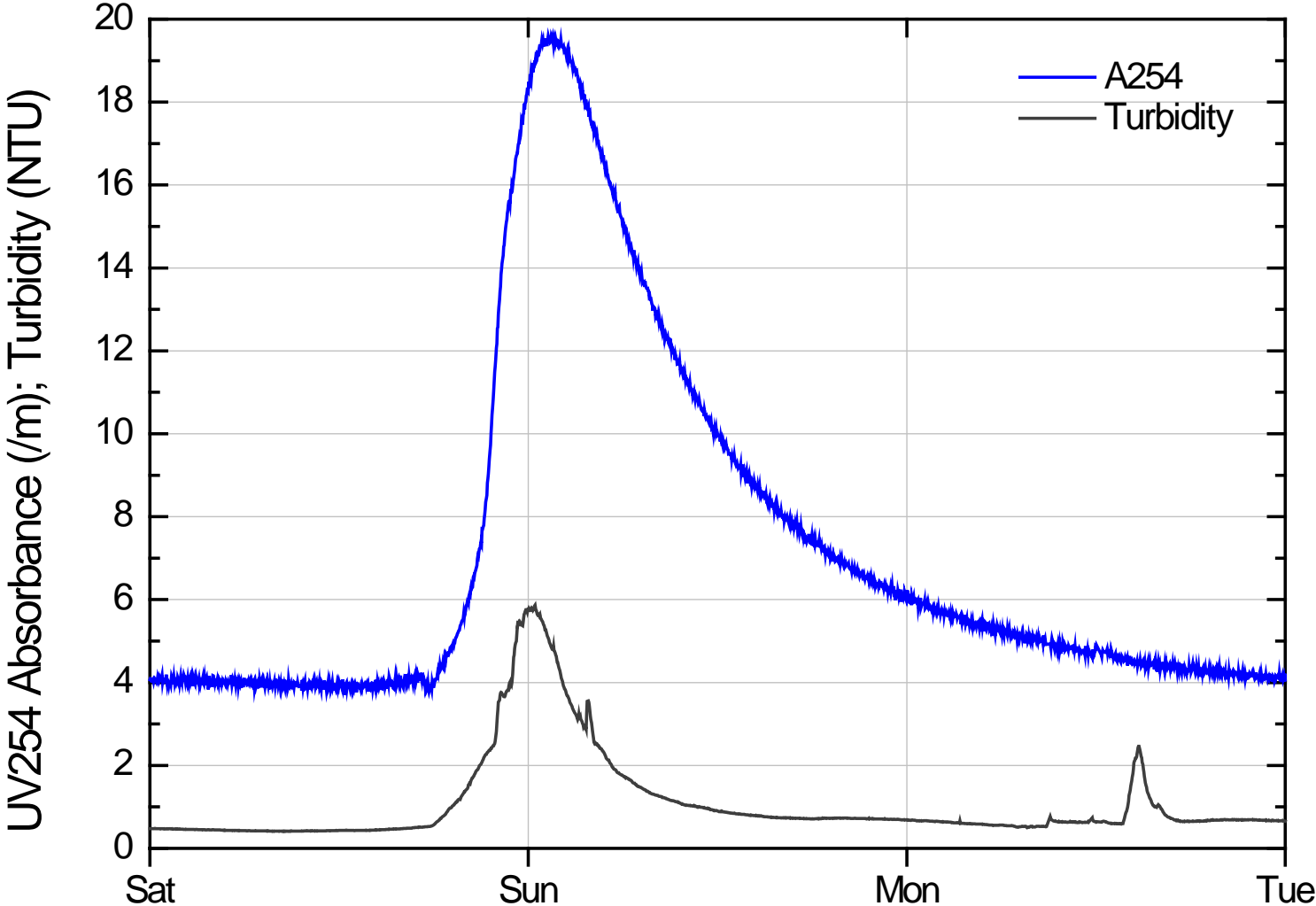
Challenges at the Plant

- Very hands on
- Overdosing of chemicals
- High production costs

Goals for the Project

- Improve control reliability
- Reduce production costs
- Reactive to proactive

Coagulant Dose Control

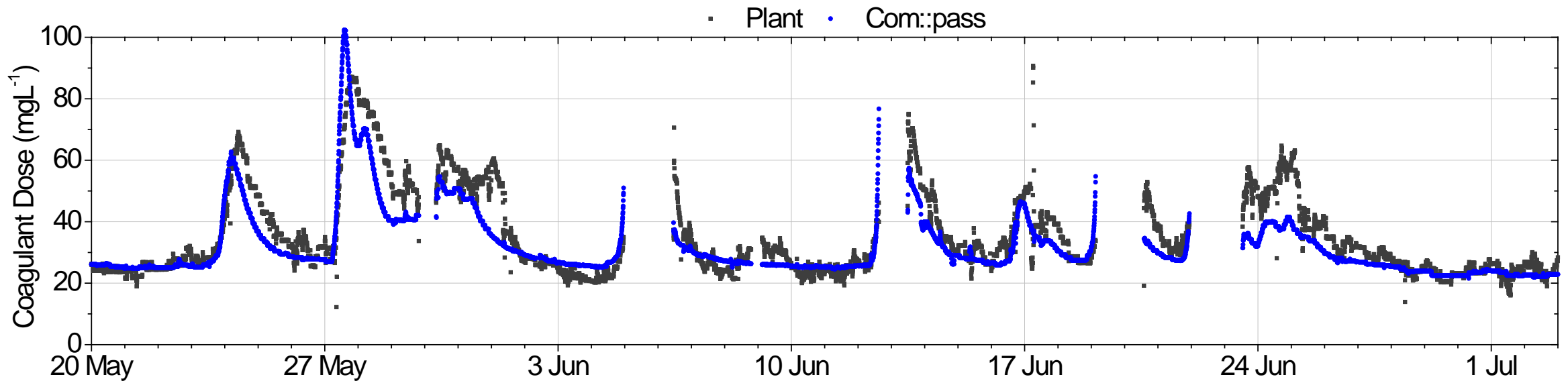






Coagulant Dose Control

- Coagulant and Lime reductions
- Filter performance improved
- More reliable



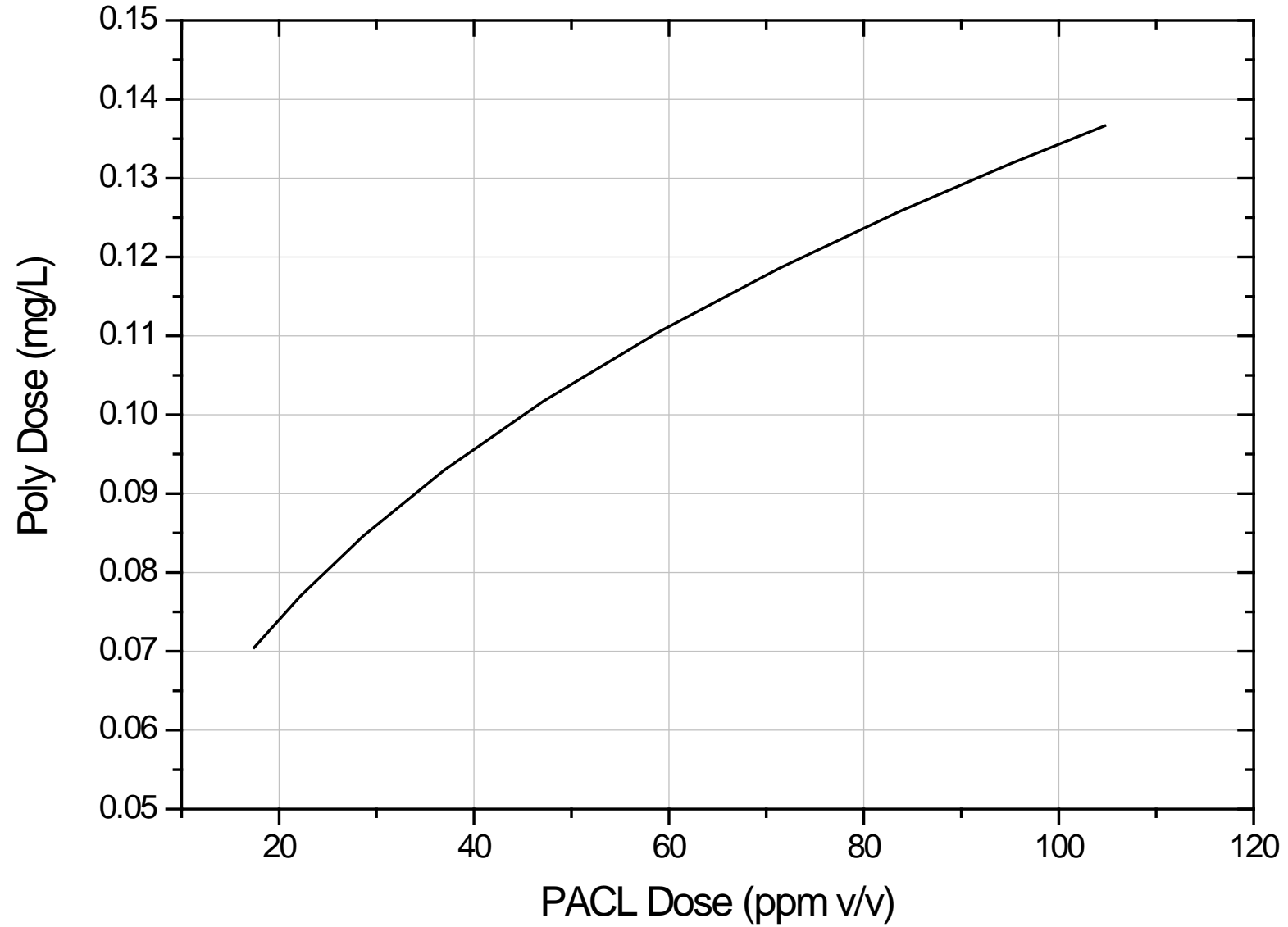
Polymer Dosing

- Setpoint control
- Too high - Carryover and filter cracking, short runtimes
- Too low – turbidity spikes
- Expensive when overdosing

To

- Automated dosing slaved off coagulant dose

Polymer Dosing



Clarifier De-sludge Control

- Time based de-sludge
- Variable solids load
- Wasting water or poor clarifier performance

To

- Load based de-sludge

Production Cost Tracking

- Bulk delivery & stock-takes
- Poor understanding
- Low transparency

To

- Online realtime production costs

Online Costs

- Chemical Costs

Equation	Description	Units
Q_{TW}	Treated water flow-rate	$m^3/h_{\text{treated water}}$
$cost_{hypo} = \$360.40$	Product cost	$\$/m^3_{\text{product}}$
Q_{hypo}	Product flow-rate from SCADA	L_{product}/h
$acost_{hypo,CWT} = \frac{24 \cdot Q_{hypo,CWT} \cdot cost_{hypo}}{100 \cdot Q_{TW}}$	Actual treatment cost	$C/m^3_{\text{treated water}}$

Online Costs

- Power costs

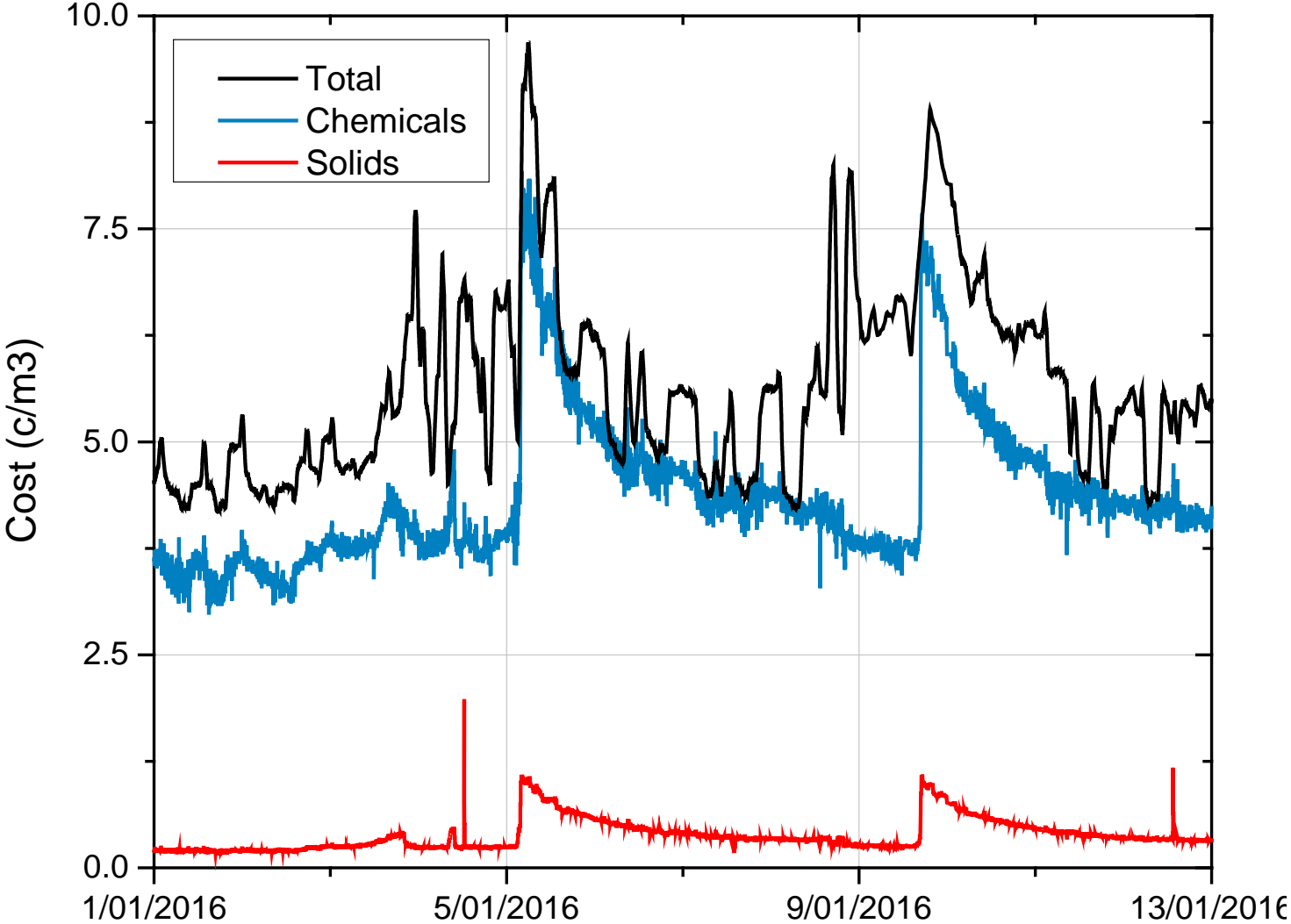


Online Costs

- Sludge disposal costs



Online Costs

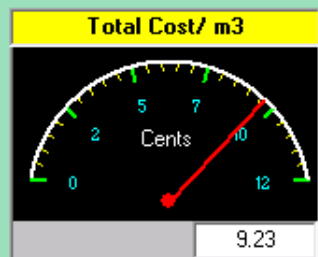


Predicted Costs & Cost Sentinel

- River and inlet monitoring
- Deviation alarms
- Cost decisions

Te Marua Online Costs

	Dose Rate	Bulk Cost	Inst.Rate	Predict Rate	Last 30min	Last 24hr
CO2 Stream 1	14.830 g/m3	383.68 \$/Ton	0.581 c/m3	0.460 c/m3	0.587 c/m3	0.587 c/m3
Lime Stream 1	12.423 g/m3	322.76 \$/Ton	0.409 c/m3	1.232 c/m3	0.404 c/m3	0.316 c/m3
Poly Stream 1	0.12 g/m3	10360.00 \$/Ton	0.123 c/m3	0.207 c/m3	0.120 c/m3	0.109 c/m3
Stream 1 PAC	0.00 g/m3	2750.00 \$/Ton	0.000 c/m3	3.300 c/m3	0.000 c/m3	0.000 c/m3
Coag Stream 1	43.553 c/m3	738.22 \$/Ton	3.937 c/m3	3.480 c/m3	4.620 c/m3	3.220 c/m3
CO2 Stream 2	0.000 g/m3		0.000 c/m3		0.000 c/m3	0.000 c/m3
Lime Stream 2	0.000 g/m3		0.000 c/m3		0.000 c/m3	0.000 c/m3
Coag Stream 2	0.000 g/m3		0.000 c/m3		0.000 c/m3	0.000 c/m3
Poly Stream 2	0.000 g/m3		0.000 c/m3		0.000 c/m3	0.000 c/m3
Total Pre-Treatment			5.180 c/m3		5.731 c/m3	4.233 c/m3
Caustic	15.16 g/m3	599.13 \$/Ton	0.971 c/m3	0.719 c/m3	0.942 c/m3	0.953 c/m3
Chlorine Gas	0.84 g/m3	2964.26 \$/Ton	0.248 c/m3	0.080 c/m3	0.252 c/m3	0.251 c/m3
Hypochlorite	0.00 g/m3	334.950 \$/Ton	0.000 c/m3	0.037 c/m3	0.000 c/m3	0.000 c/m3
Fluoride	0.801 c/m3	1650.00 \$/Ton	0.134 c/m3	0.179 c/m3	0.134 c/m3	0.136 c/m3
Total Post Treatment			1.351 c/m3		1.328 c/m3	1.340 c/m3
Hutt River Predicted				0.000 c/m3	0.000 c/m3	0.000 c/m3
Plant Intake Predicted				10.751 c/m3	10.701 c/m3	9.610 c/m3
Inlet Dried Solids	15.817 g/m3					
Thickner Poly			0.033 c/m3		0.032 c/m3	0.023 c/m3
Centrifuge Poly			0.251 c/m3	0.000 c/m3	0.243 c/m3	0.173 c/m3
Solids Disposal		110.00 \$/Ton	0.888 c/m3		0.861 c/m3	0.612 c/m3
Power Price	11.41 c/kWhr					
Plant Power			0.473 c/m3		0.447 c/m3	0.566 c/m3
Boost Pumps			1.056 c/m3		0.958 c/m3	0.854 c/m3
Treatment Pumps			0.000 c/m3		0.000 c/m3	0.000 c/m3
PAT Saving			0.000 c/m3		0.000 c/m3	0.000 c/m3
Totals						
Total Chemical			6.532 c/m3		7.059 c/m3	5.573 c/m3
Total Power			1.509 c/m3		1.406 c/m3	1.419 c/m3
Total Solids			1.144 c/m3		1.136 c/m3	0.808 c/m3
All Cost Total			8.941 c/m3		9.601 c/m3	7.800 c/m3



Typical Dose Rates			
CO2	PAC	CL2	FL
12.000 %/vol	12.000 g/m3	0.800 g/m3	0.750 g/m3

Calibration Factors	
Lime Feeder A	1.0700
Lime Feeder B	1.0700
Lime Feeder C	
Poly Strength	0.30 %w/vol
Hypo Strength	0.77 %w/vol
Plant Recovery	98.0 %
Thickner Dose	2.0 kg/TonDS
Cent. Dose	15.0 kg/TonDS
Sludge Cake DS	20.00 % w/v

Trends	
	Plant Volumes
	Stream 1
	Stream 2
	Post Treatment
	Solids
	Power
	Totals

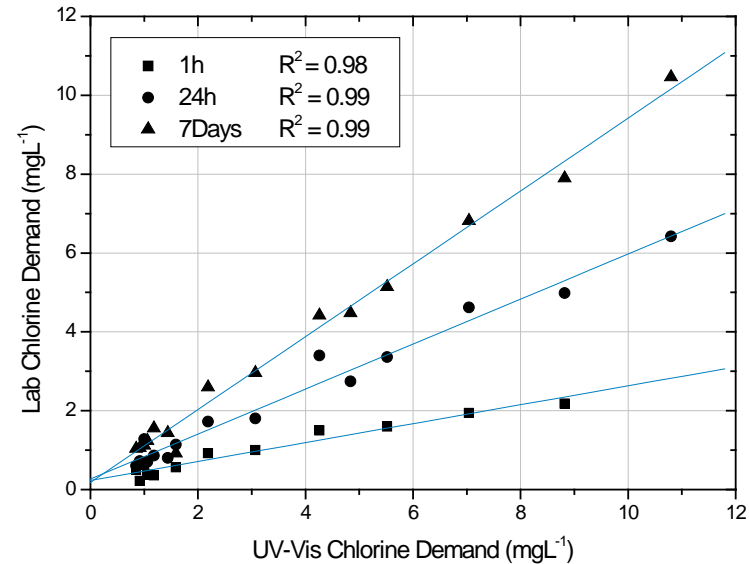
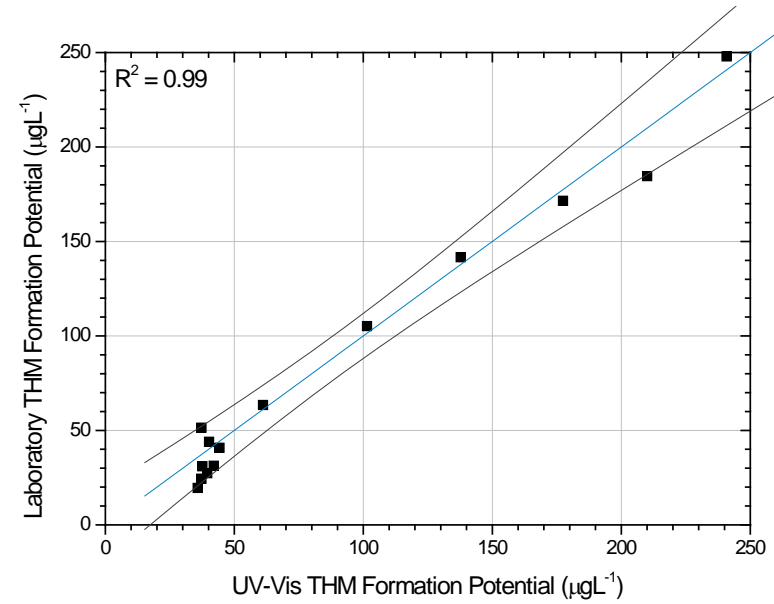
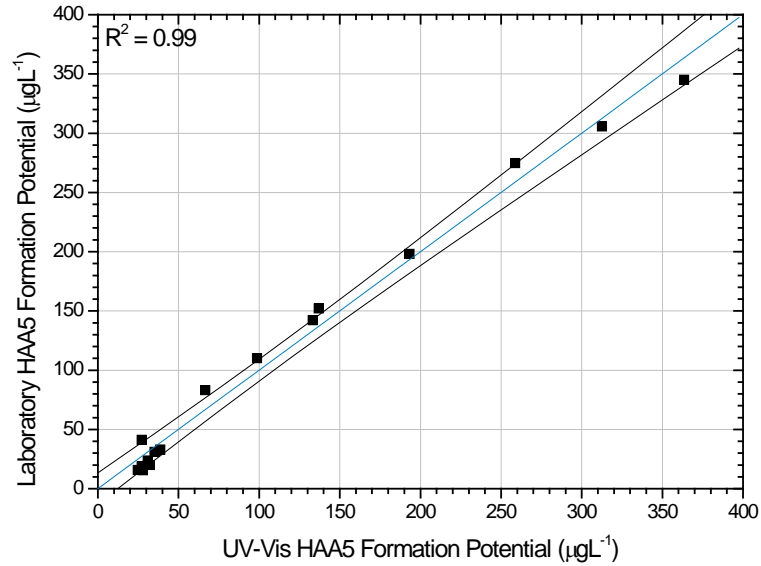
Alkalinity Control

- Manual CO₂ dose control
- Variable treated water alkalinity

To

- Feed forward alkalinity control
- Tightly controlled treated water alkalinity

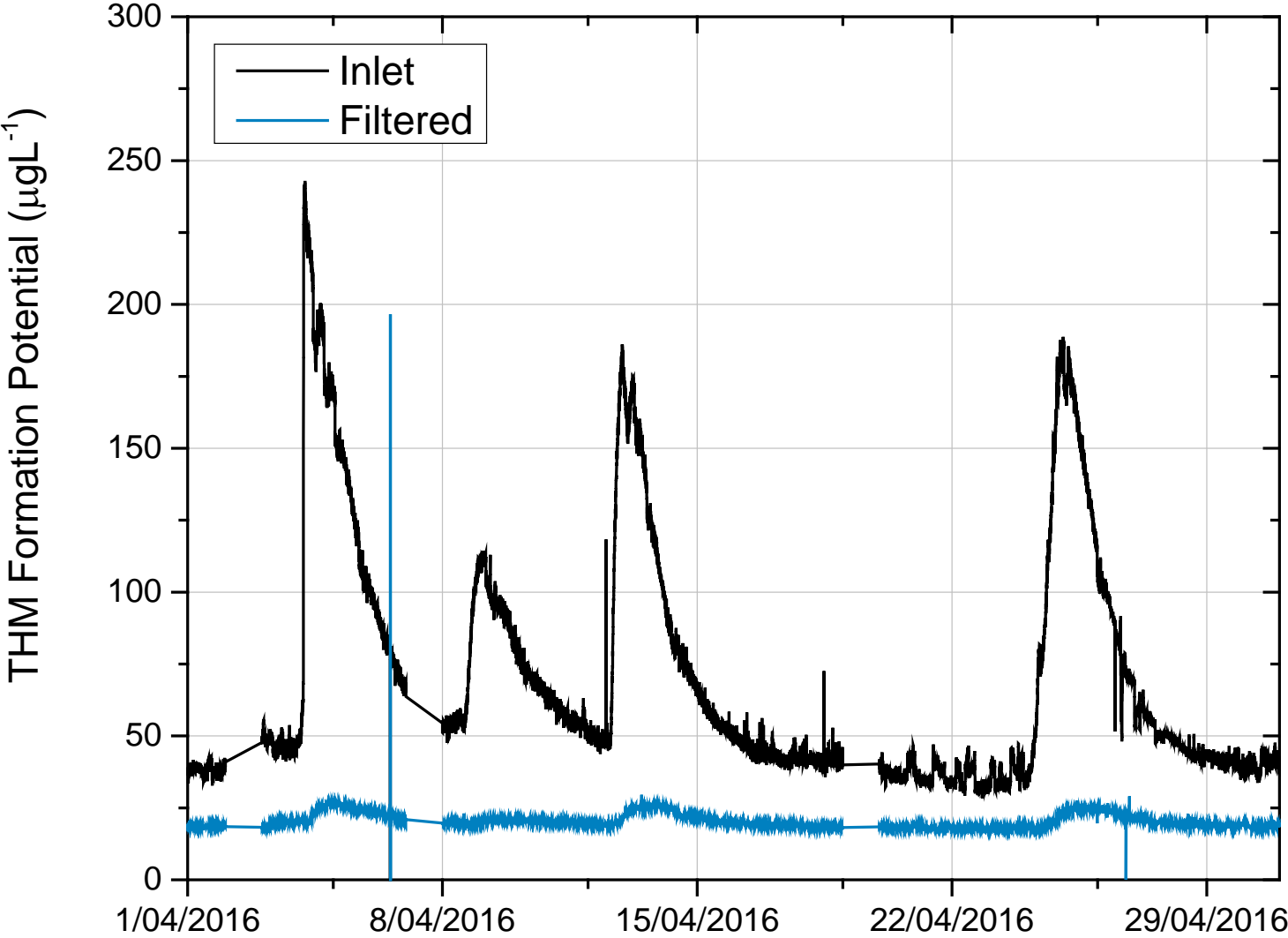
Chlorine Demand and THM/HAA FP



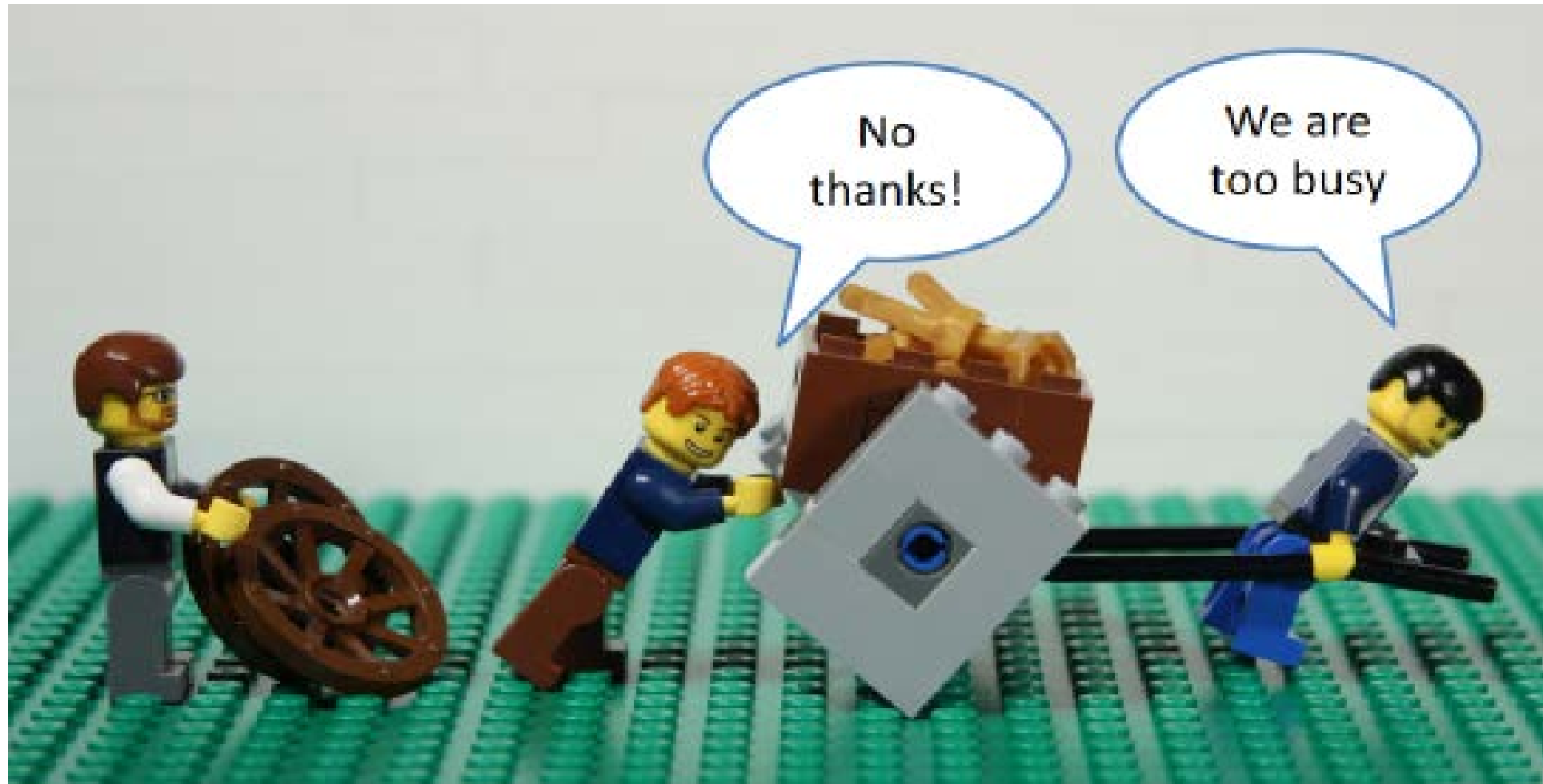
Chlorine Demand and THM/HAA FP

- Online Measurement
- P2 risk reduction
- Optimisation potential

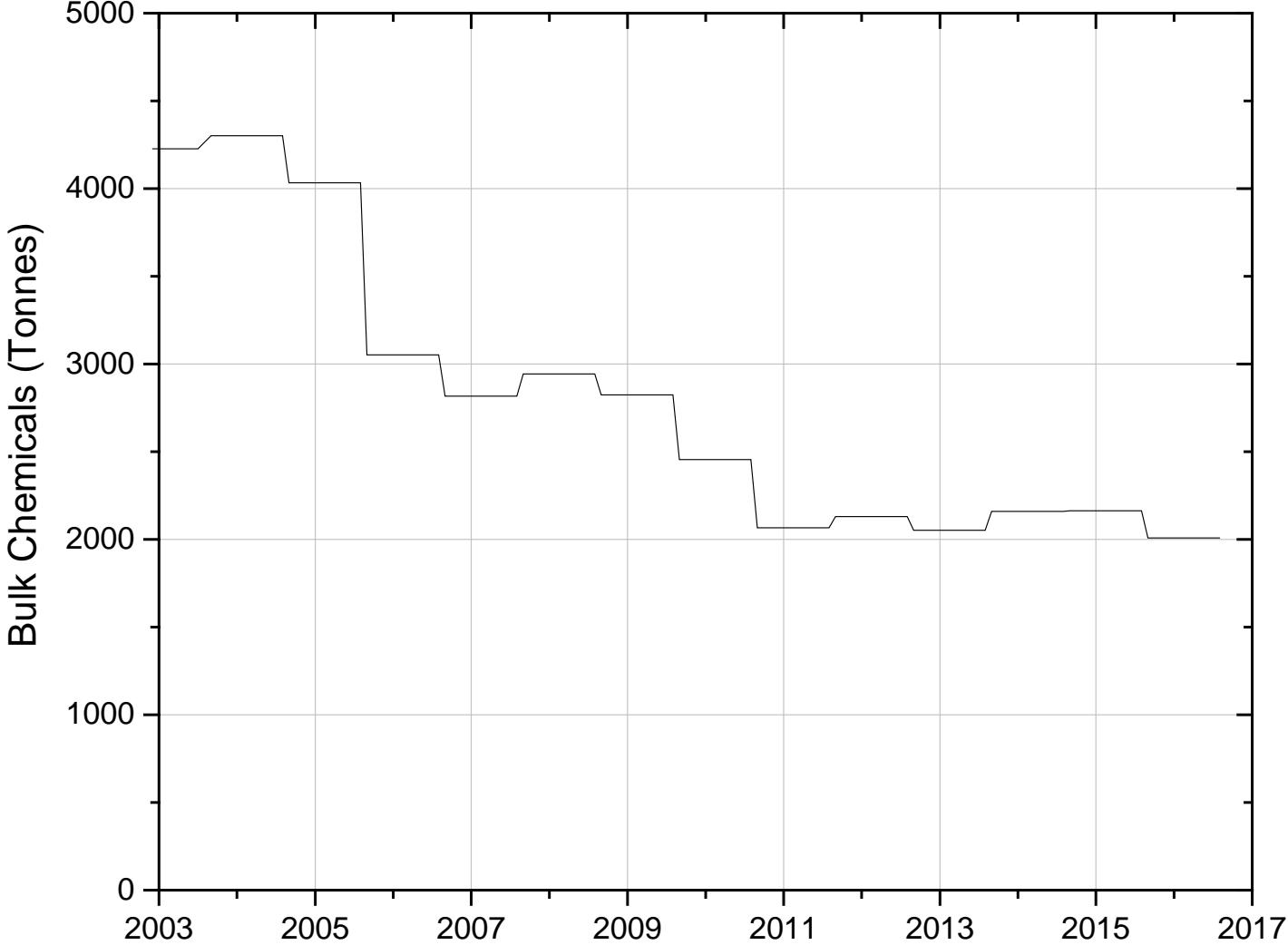
Enhanced Organics Removal



Conclusion



Conclusion



Questions?

